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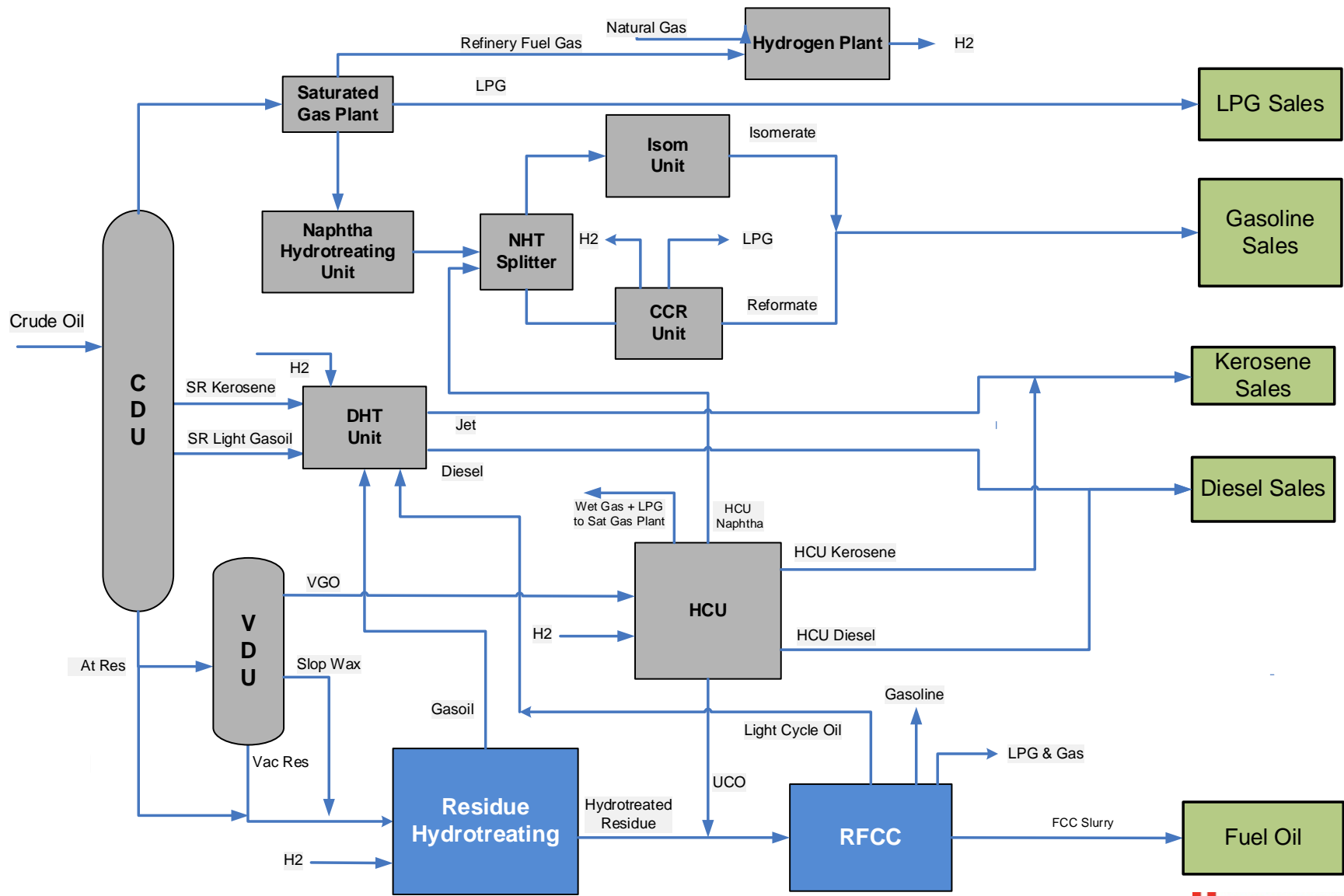
# Upgrading Fuel Oil to Euro V Gasoline

Residue Hydrotreating and RFCC

5<sup>th</sup> December 2017 | Bottom of the Barrel Workshop | NIORDC, Tehran



# RCD Unionfining – RFCC Complex



# Agenda



Challenges in upgrading residue streams



Impact of heavy feeds on RFCC operation and conversion



RCD Unionfining™ process enables efficient downstream upgrading



UOP RFCC Process: technology solution for economic upgrading of residue to gasoline

# Residue Streams are Challenging to Process

- Contaminant levels increase with boiling range in most crudes
- Residue streams typically contain high sulphur, nitrogen, Conradson carbon, organometals and asphaltenes

Stream	Atmospheric Residue	Vacuum Residue
Sulphur, ppm wt	2.3	3.0
Nitrogen, ppm wt	<b>2600</b>	<b>4000</b>
Conradson Carbon, %wt	<b>8</b>	<b>16.3</b>
Ni + V, ppm wt	<b>83</b>	<b>164</b>
Asphaltenes, %wt	<b>1.5</b>	<b>3.1</b>

**Key to success is managing pressure drop**



# Impact of Residue Feeds on RFCC Unit Operation

1. **UOP K Factor:** The K factor differentiates between the paraffinicity and aromaticity of the feed, and it indicates the crackability of the feed
2. **Sulphur:** Increases the sulphur content of the products
3. **Nitrogen:** Basic nitrogen compounds will neutralize acid sites on the catalyst causing temporary loss of catalyst activity and drop in unit conversion
4. **Conradson Carbon:** Increases coke yield and could limit the coke burn capacity
5. **Metals Content:** All metal contaminants have a negative impact on catalyst performance. Vanadium deactivates the catalyst by destroying the zeolite crystal structure. Nickel promotes dehydrogenation reactions
6. **Hydrogen in Feed:** drives conversion and higher propylene yields

Impact can be managed by residue hydrotreating

# RCD Unionfining™ Process

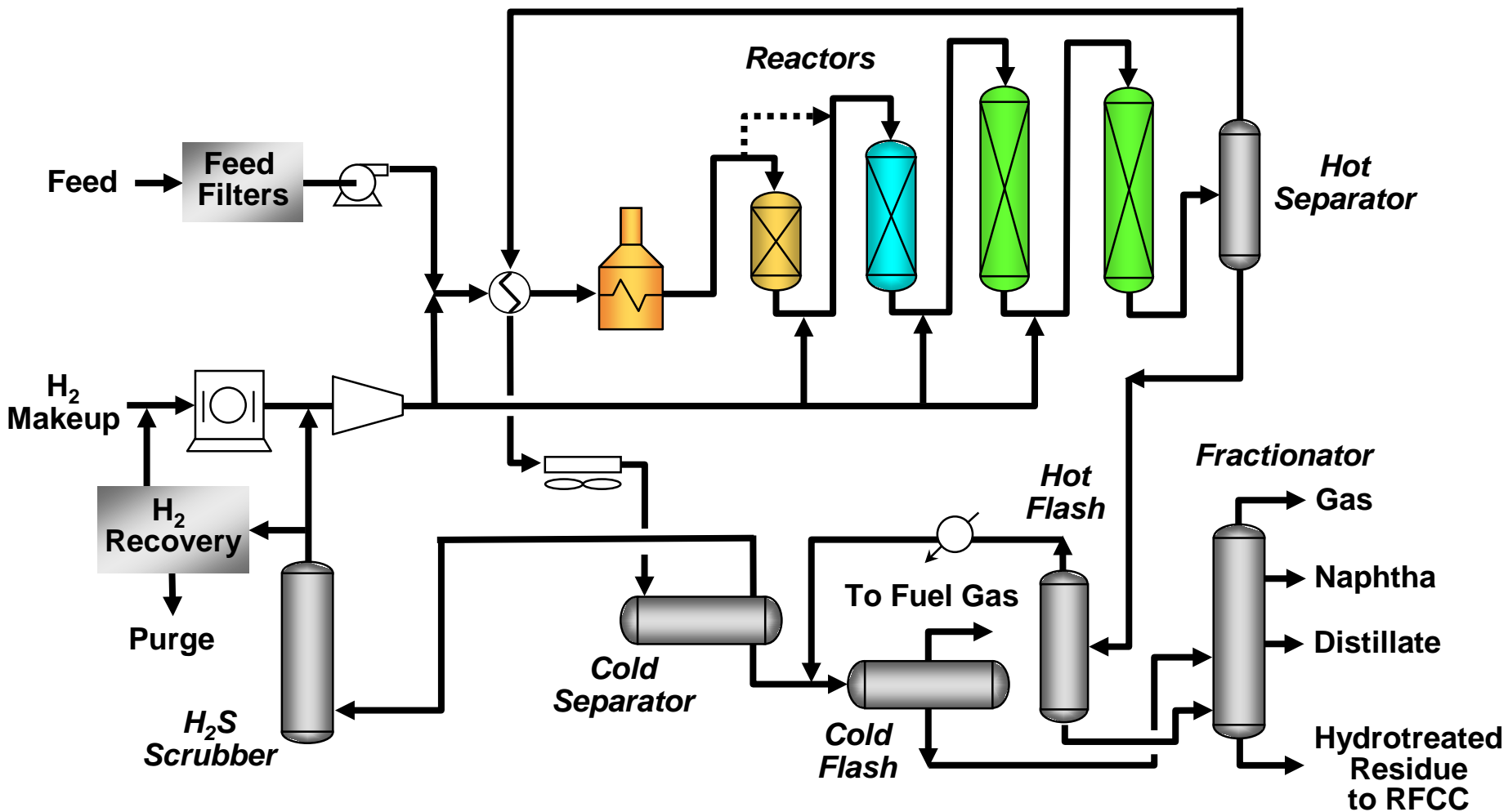
- UOP's licensed residue hydrotreating technology for processing highly-contaminated feedstocks such as AR, VR and DAO
- Combines commercially-proven process technology, proprietary catalyst systems and proprietary reactor internals
- Reduces the contaminant (sulfur, nitrogen, Conradson carbon, asphaltene and Ni+V) contents of feedstocks and adds hydrogen to produce:
  - low sulfur fuel oil
  - upgraded feedstocks for conversion units (FCC, RFCC, Coker, Hydrocracker)
- RCD Unionfining unit commercial experience:
  - First unit licensed in 1967
  - >30 units licensed with a combined capacity of >1,000,000 BPSD

# RCD Unionfining Process – Commercial Experience

- Commercial flow schemes include:
  - Single- and two-stage configurations
  - Single- and parallel-reactor trains
  - Stripper or full fractionation configurations
- Feedstock qualities of commercial RCD Unionfining process units:
  - °API: 9 - 18
  - Sulfur: 3 - 5 wt%
  - Conradson Carbon: 5 - 15 wt%
  - Organometallics (Ni+V): 10 - 200 ppm wt
  - Viscosity: 25 - ~1000 cSt@100°C
- Operating conditions of commercial RCD Unionfining process units:
  - Throughput: 5600 - 75,000 BPSD
  - Pressure: 80 - 205 barg
  - LHSV: 0.10 - 1.2 hr<sup>-1</sup>
  - Operating cycles: 6 - 24 months (typical economic optimum ~12 months)

**Operating conditions tailored to each application**

# RCD Unionfining Process – Typical Flow Scheme



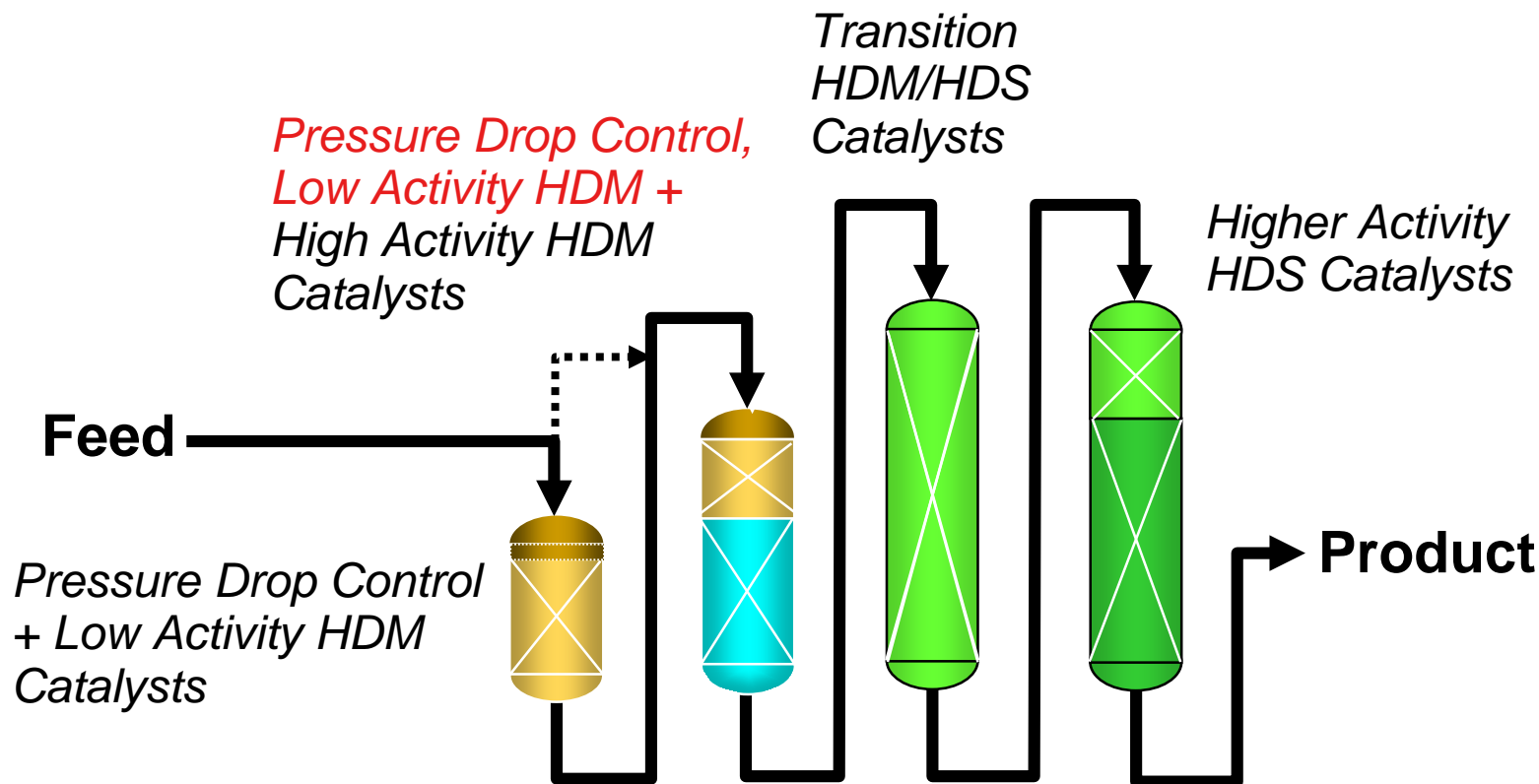
Number of reactors depends on specific service



# Specialist Catalyst Systems

- Over 120 catalyst loadings
- Proprietary catalysts designed for specific functions:
  - Pressure drop control – high efficiency particulate traps
  - Metals removal / accumulation
  - Metals removal / desulfurization
  - Conradson carbon reduction
  - Desulfurization
- Pilot plant facilities available to verify estimated performance, produce product samples, etc.

# Optimized Catalyst Loading



**Tailored catalyst loadings optimise residue hydrotreating unit performance and economics**

# RCD Unionfining Process Summary

- RCD Unionfining Process enables efficient upgrading of residue streams via RFCC
  - Reduces metals, Conradson carbon, sulphur, nitrogen and asphaltenes
  - Adds hydrogen → higher RFCC conversion and gasoline yield
- Specialist process design & catalyst system required to achieve good cycle length
- Processing targets need to be optimised together with RFCC operation considering
  - Overall capital cost
  - Overall yields
  - Operating costs (including hydrogen & catalysts)

# Agenda – Residue FCC



Economic Drivers for  
RFCC Units



Impact of heavy feeds  
on RFCC Unit  
conversion



UOP RFCC Process:  
meet economic  
objectives with  
technology solutions



# RFCC Operating Modes

## Distillates Mode RFCC

- Maximum LCO yield
  - ◆ Extremely Low Cetane Number ~ 19-20
  - ◆ Challenging to route LCO to EURO 5 diesel

## Conventional RFCC (Fuels)

- Gasoline and LPG
  - ◆ 4-6 wt% propylene
  - ◆ 50-58 wt% gasoline
- Typical catalyst system and operating conditions

## Fuels and Petrochemicals (Enhanced LPG)

- Gasoline/Alkylate/Petrochemicals
  - ◆ 6-12 wt% propylene
  - ◆ 38-48 wt% gasoline
- Catalyst system with ZSM-5 and modified operating conditions

## Petrochemicals (High Propylene)

- 12+ wt% propylene
- Catalyst system with ZSM-5
- Optimized process conditions (pressure, temp, steam)
- Poor quality of naphtha & LCO - challenging to route to EURO 5 gasoline & diesel



**Solution**

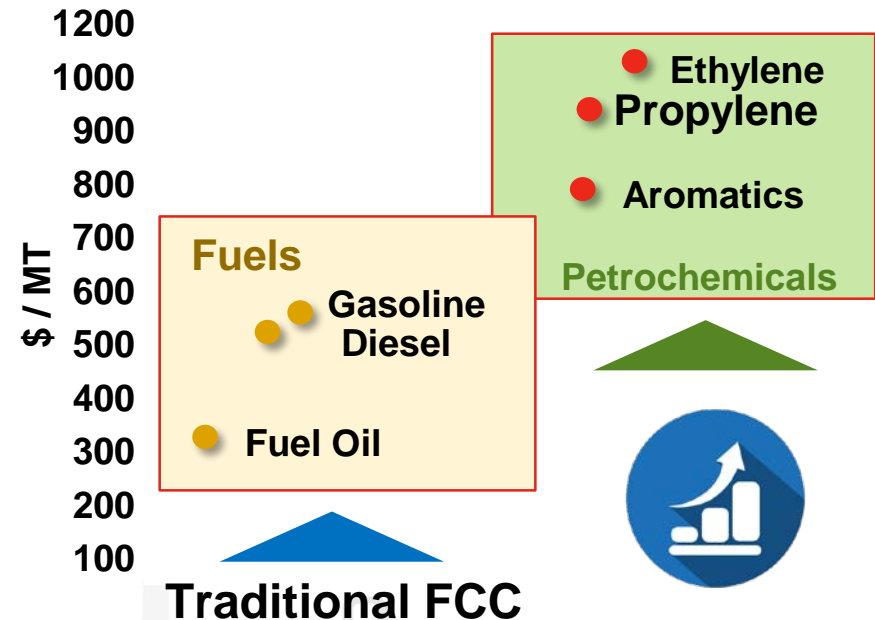
*Distillate Mode: Cost to upgrade low cetane LCO negatively impacts economics*

# RFCC Drivers to Capitalize new Opportunities

UOP RFCC specifically designed to help maximize value by:

- Producing **higher value product – propylene**
  - Ability to produce **polymer grade propylene** (e.g.- 250+ KMTA from 2.5M MTA RFCC)
- **Simultaneously** helping to maximize RFCC naphtha as a gasoline blendstock whilst making propylene
- **Class V compliant with 95 RON (low enough aromatics to blend to gasoline)**
- Unmatched licensing experience
  - 295 units licensed
  - More than 50% of world-wide capacity
  - 70 years of design & operation feedback

Product Prices, September 2017

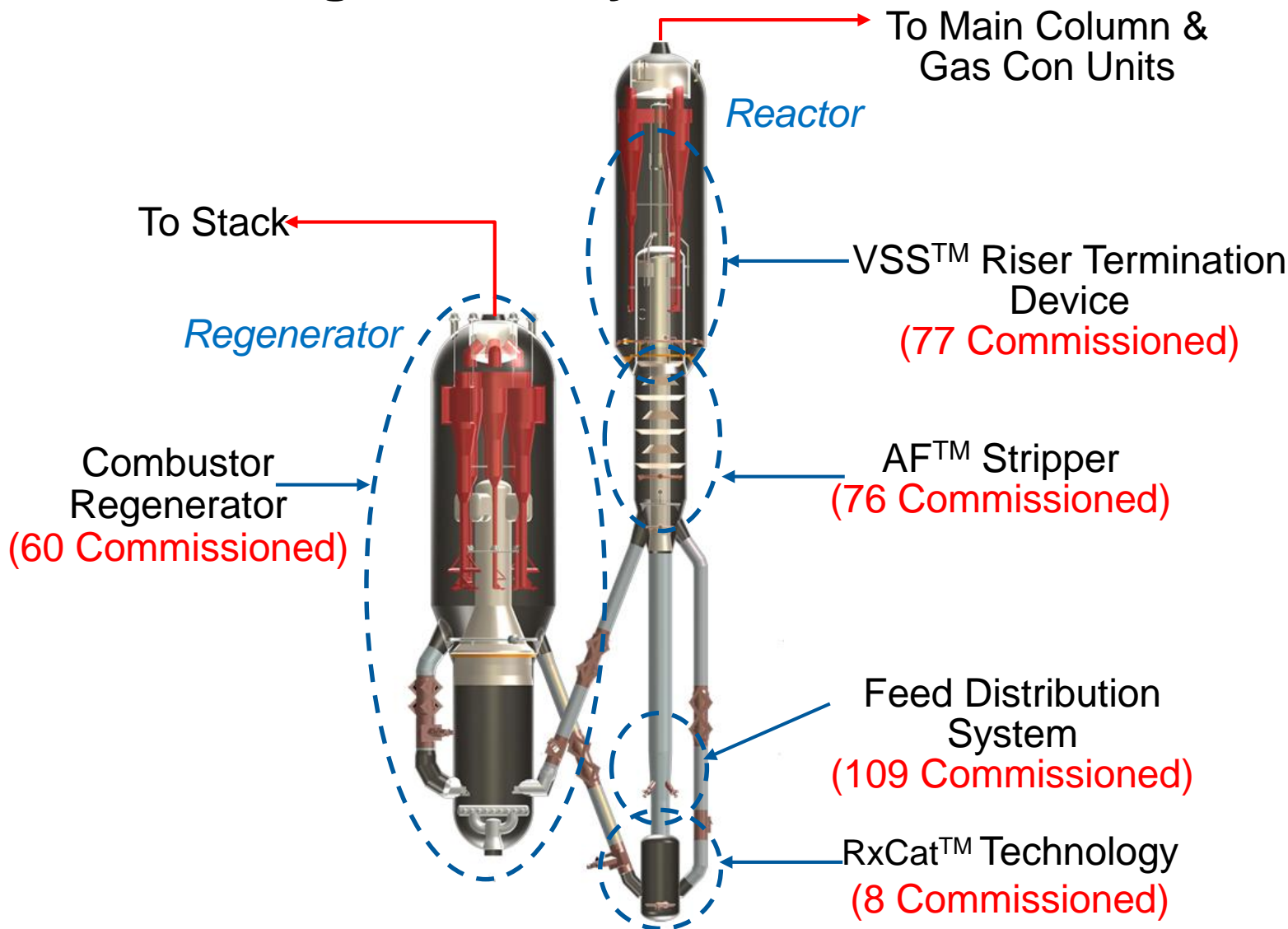


➔ Shift to petrochemicals adds significant value

Enhanced LPG RFCC significantly improves project economics



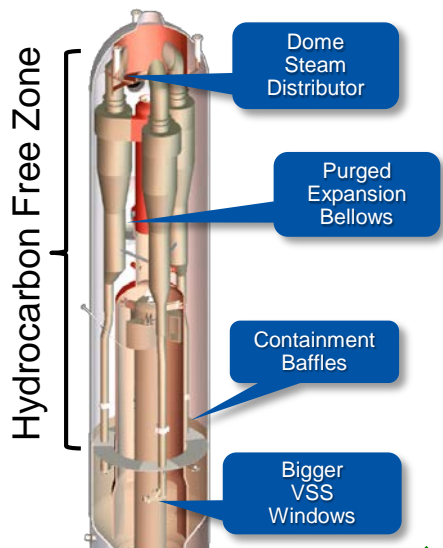
# Best in Class FCC Technologies Maximize Processing Versatility and Yields



**Fully commercialised technology**

# Technology options for improved yields and economics.

### VSS™ Riser Termination



Hydrocarbon Free Zone

- Gasoline Selectivity
- Dry Gas,  $\Delta$ Coke, Trg
- Improved Reliability
- 77 Commissioned

### AF™ Stripper Packing



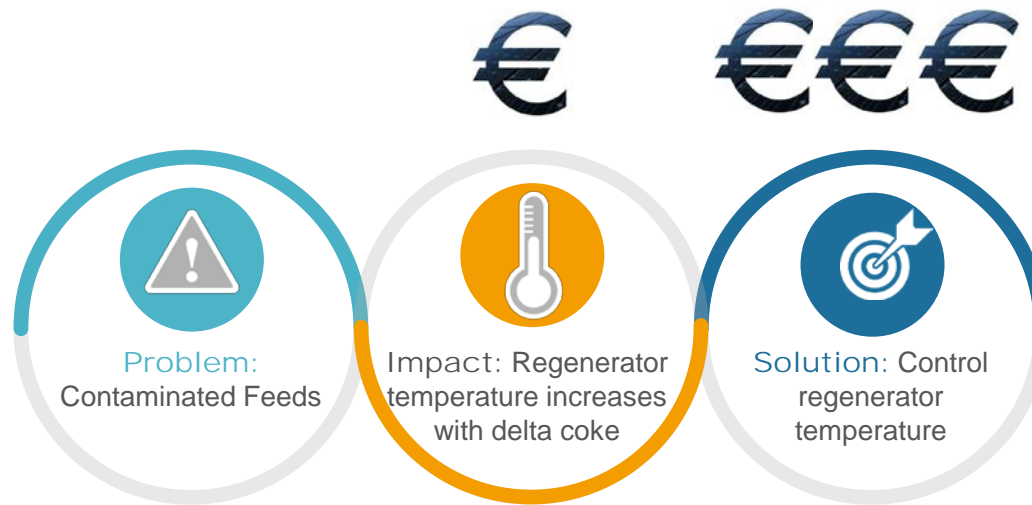
- Conversion
- Dry Gas,  $\Delta$ Coke, Trg
- Improved Reliability
- Improved Ops Flexibility
- 14 Commissioned

### Elevated Feed Distributors



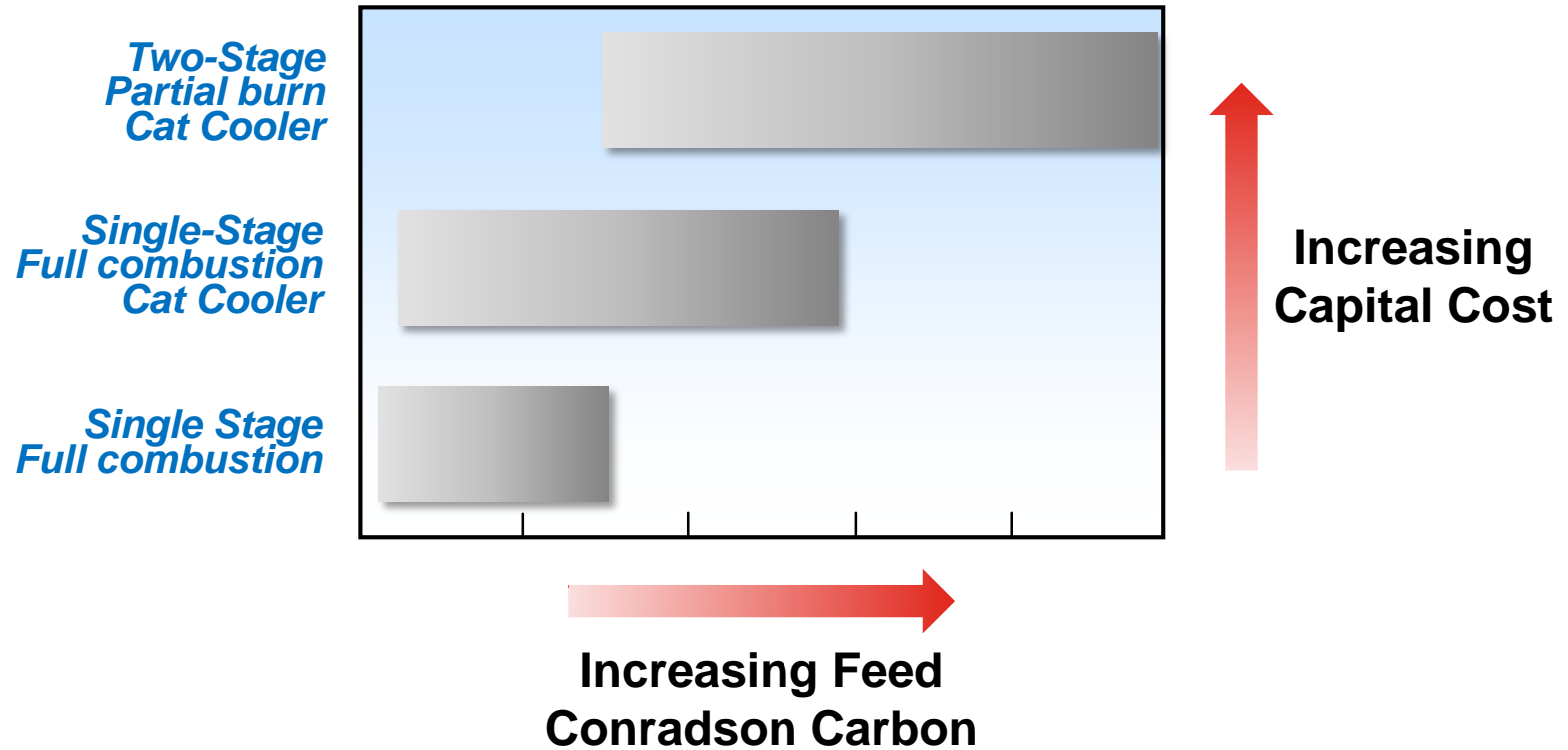
- Conversion
- Gasoline Selectivity
- Dry Gas,  $\Delta$ Coke, Trg
- Improved Reliability
- 109 Commissioned

# Options Available for Handling Increased Coke Formation



- High Delta Coke
  - Catalytic coke
  - [Contaminant coke](#)
- Reduces C/O and conversion
  - Accelerated catalyst deactivation
  - Decreased internal equipment working life
  - [Low product margins](#)
- Inclusion of latest technology that minimize delta coke
  - Catalyst cooler
  - Partial combustion operation, application of Two-Stage Regenerator
  - [High product margins](#)

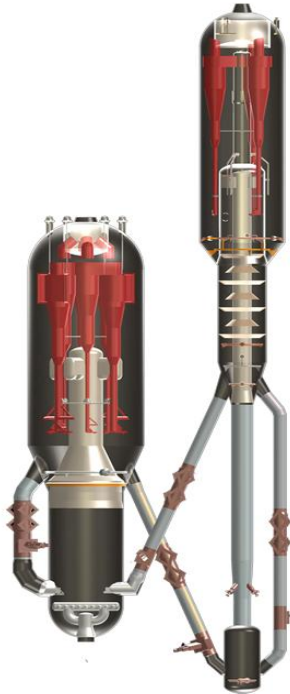
# UOP's RFCC Regenerator Technology Portfolio



UOP Technology can process a wide range of feed Conradson Carbon

# UOP's RFCC Regenerator Technology

## Single Stage Combustor



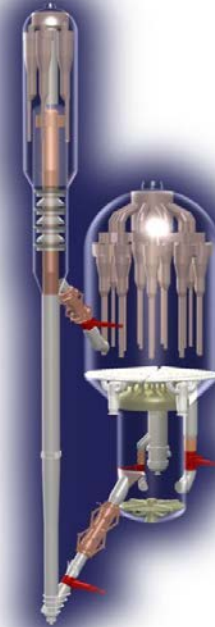
### Single Stage – Combustor Operation

- Full combustion (Single Stage Combustor) is simpler approach
  - No CO Boiler required
  - Lower cost flue gas section
- Regenerator operating temperature managed with catalyst cooler
  - For temperature  $>732^{\circ}\text{C}$

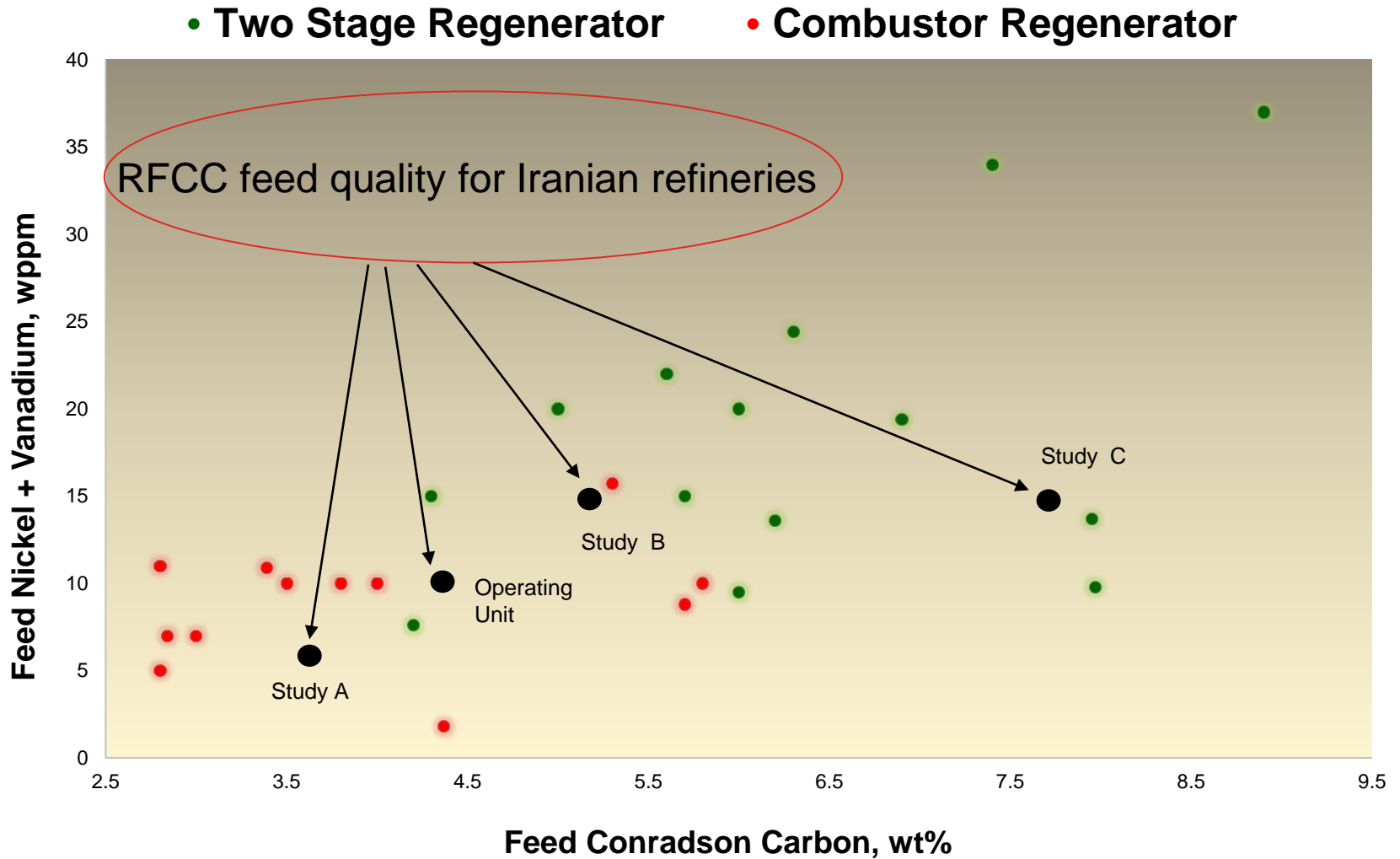
### Traditional Two Stage – Partial Combustion

- Partial mode of operation
- Compared to other Two Stage Regenerator style, UOP design offers:
  - Single flue gas line
  - Easier for power recovery

## Traditional Two Stage Partial Combustion

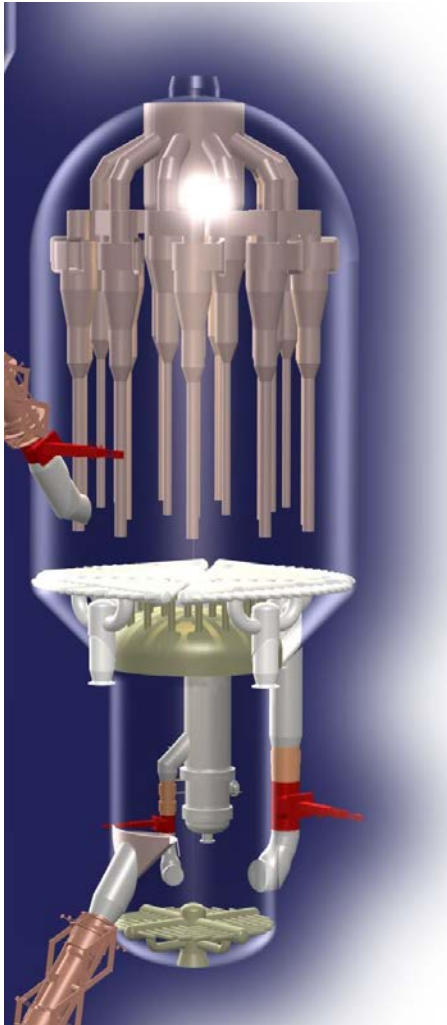


# Significant Experience with Highly Contaminated Residue





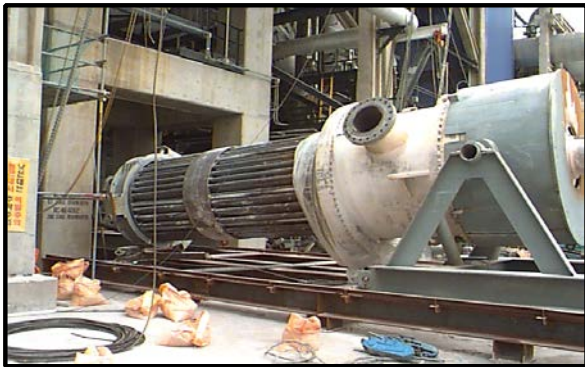
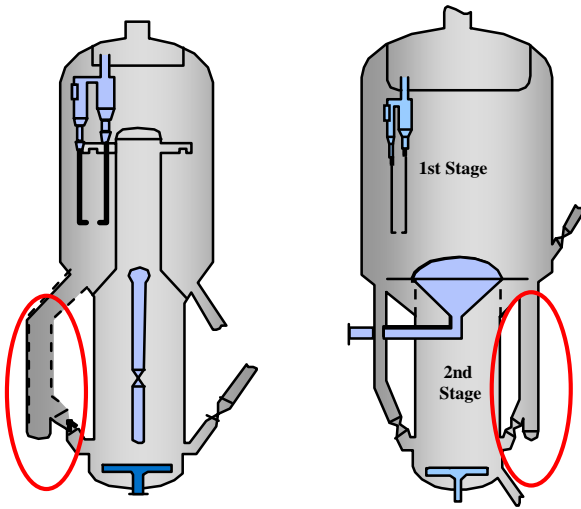
# UOP Two-Stage Regenerator



- To burn high delta coke on catalyst and process highly contaminated feed
- Partial combustion operation
- Proven on feeds of ~10 Wt-% concarbon and 20,000 wppm Ni+V on catalyst
- Maximizes oxygen utilization
  - Excess oxygen in 2nd stage flue gas is used to burn coke in 1st stage
  - Minimizes air blower capacity
  - Single flue gas system
- Operator friendly
  - Result of stacked design and trouble free catalyst circulation
  - Responds well to upsets and turndown

**Lowest Capex/Opex solution for contaminated feeds**

# Processing Heavier Feeds in an RFCC



## *When is a Catalyst Cooler Needed?*

- Regenerator temperature too high (> 732°C / 1350°F)
- Process residue feedstocks with high Conradson Carbon (Concarbon)

## *What Does a Catalyst Cooler Do?*

- Removes large amounts of heat from regenerator
- Generates HP steam

## *What is the Result?*

- Regenerator temperature is reduced and independently controlled
- Cat/oil ratio increases
- Lower catalyst deactivation rate
- Improves conversion and product yields

**Commercially proven technology to increase product revenues**

# Case Study – NE Asia FCC Unit

## *Revamp basis*

- Operation: 53,000 BPSD VGO+AR feed in gasoline mode
- Current configuration: UOP FCC with Combustor style regenerator
- Revamp objective: Increase conversion with same feed blend

## *Revamp scope Add single UOP Catalyst Cooler*

## *Result*

- Total annual benefit = \$18 MM/yr

**Approximately 1 year simple payback**

# Case Study – RFCC operates with one of the world's most difficult Feed

- **Design**

- 75,000 BPD 100% AR Oman crude
- RFCC with Two-Stage regenerator
- 18.2 API, 6.9 wt% Con Carbon, 9 wppm Nickel, 10 wppm Vanadium
- 9 wt% propylene

- **Commissioned in 2006**

- Poorer quality feedstock – more contaminated than design
- Some initial equipment and operation issues
- 17.3 API, 8.9 wt% Con Carbon, 20 wppm Nickel, 17 wppm Vanadium
- 8 wt% propylene
- Up to 110% capacity on more difficult feedstock

- **Recent operation**

- Con Carbon 8.5 to 9.5 wt%
- Total feed metals to 44 wppm ~ 50/50 Nickel and Vanadium
- Ecat metals around 14,000 wppm (about 7000 ppm each)



**Unit has achieved C3= yield >8 wt%**

# Conclusions



Iranian Refiners have an **incentive to process heavier feeds** in RFCC Units that are heavily contaminated by metals and CCR and require a robust technology



UOP's RFCC technology **solutions** designed to handle feeds with a broad range of Conradson carbon and Metals



UOP's RFCC helps **maximize conversion & yield selectivity**; is flexible, proven & extensively commercialized



UOP's RFCC technology has **successfully been proven with one of the world's most difficult feed** achieving C3= yield of 8 wt. %

